Upgrading Process of 4-Methylanisole as a Lignin-Derived Bio-Oil Catalyzed by Pt/γ-Al₂O₃: Kinetic Investigation and Reaction Network Development

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This document includes the following Table and Figures:

Table S-1: Overall mass balance closure data.

Figure S-1: Selectivity for the formation of the following products in the conversion of 4-methylanisole catalyzed by $Pt/\gamma Al_2O_3$ in the presence of H_2 at T = 623 K and P = 8 bar. Data for each main product were fitted with a straight line and extrapolated to zero conversion; intercepts of regression lines significantly different from zero selectivity at zero conversion indicate primary products.

Figure S-2: Selectivity for the formation of the following products in the conversion of 4-methylanisole catalyzed by $Pt/\gamma Al_2O_3$ in the presence of H_2 at T = 673 K and P = 8

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bar. Data for each main product were fitted with a straight line and extrapolated to zero conversion; intercepts of regression lines significantly different from zero selectivity at zero conversion indicate primary products.

Figure S-3: Conversion to each of the main products as a function of inverse space velocity at 623 K and 8 bar; the term X_i represents the conversion to product i.

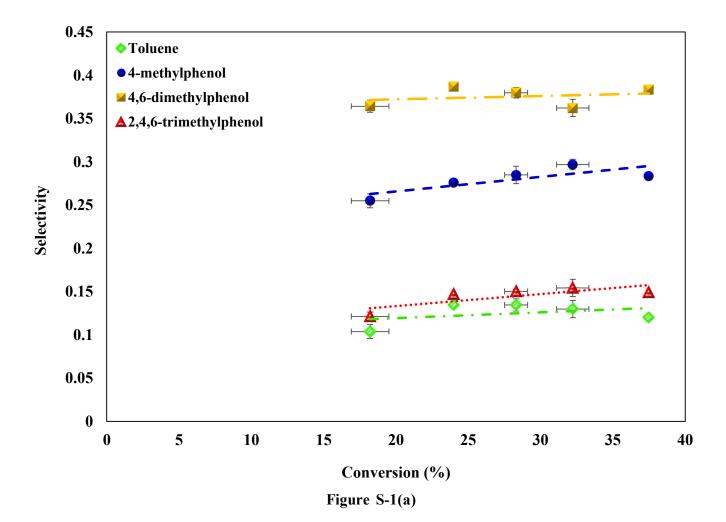
Figure S-4: Conversion to each of the main products as a function of inverse space velocity at 673 K and 8 bar; the term X_i represents the conversion to product i.

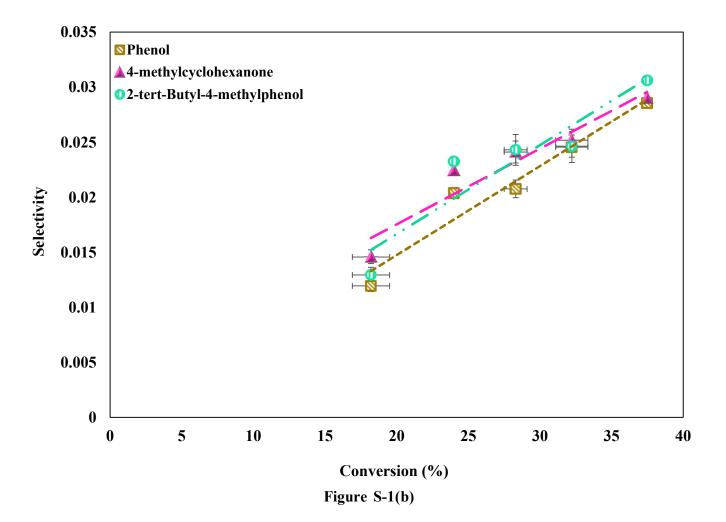
Figure S-5: Conversion of 4-methylanisole in the presence of H_2 at T=623 K and P=8 bar to give main products, where X_i is conversion of 4-methylanisole on a logarithmic scale.

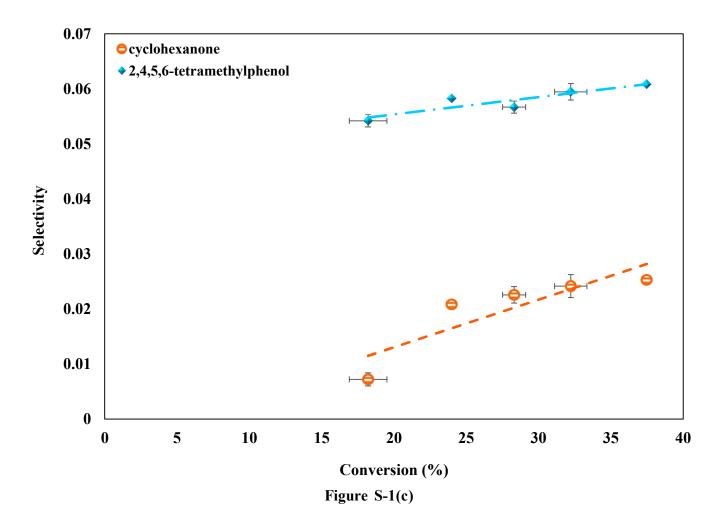
Figure S-6: Conversion of 4-methylanisole in the presence of H_2 at T=673 K and P=8 bar to give main products, where X_i is conversion of 4-methylanisole on a logarithmic scale.

Table S-1

Experiment number	Mass balance closure (%)	Time on stream (min)	Liquid flow rate (mL/min)	Mass of liquid fed (g)	Mass of liquid collected from condenser (g)	Mass of reactant leaving condenser as vapor (g)	Approximate mass of liquid remaining in condenser (g)
1	97.56	150	0.1	14.54	12.97	0.21	1
2	98.04	150	0.1	14.54	13.02	0.23	1
3	97.49	150	0.1	14.54	12.98	0.19	1
4	99.90	150	0.1	14.54	13.29	0.23	1
5	98.86	150	0.1	14.54	13.15	0.22	1
6	96.80	150	0.1	14.54	12.87	0.2	1
7	100.38	150	0.1	14.54	13.38	0.21	1
8	97.81	180	0.05	8.72	7.38	0.15	1
9	98.38	180	0.05	8.72	7.43	0.15	1
10	97.24	180	0.05	8.72	7.35	0.13	1
11	99.87	180	0.05	8.72	7.57	0.14	1
12	98.73	180	0.05	8.72	7.46	0.15	1
13	99.07	180	0.05	8.72	7.49	0.15	1
14	95.98	180	0.05	8.72	7.21	0.16	1
15	97.24	180	0.05	8.72	7.34	0.14	1
16	98.61	360	0.03	10.47	9.16	0.16	1
17	97.94	360	0.03	10.47	9.08	0.17	1
18	98.71	360	0.03	10.47	9.16	0.17	1
19	97.94	360	0.03	10.47	9.09	0.16	1
20	100.24	360	0.03	10.47	9.31	0.18	1







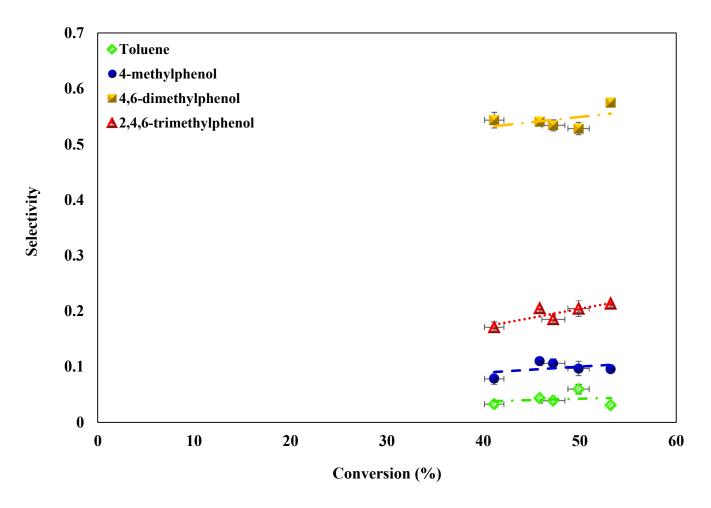


Figure S-2(a)

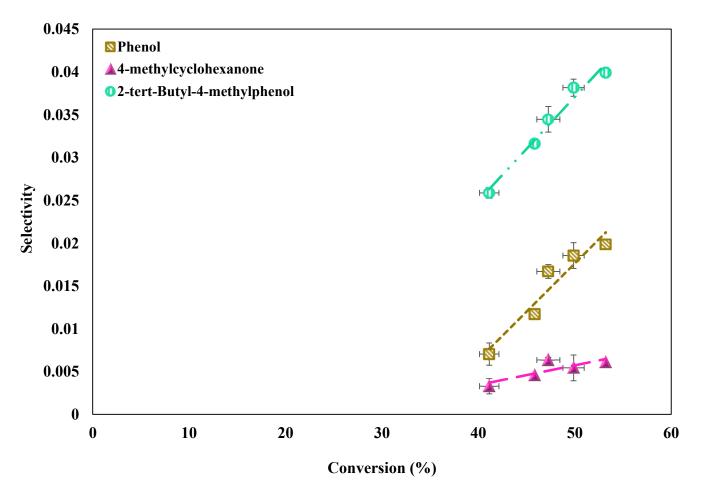
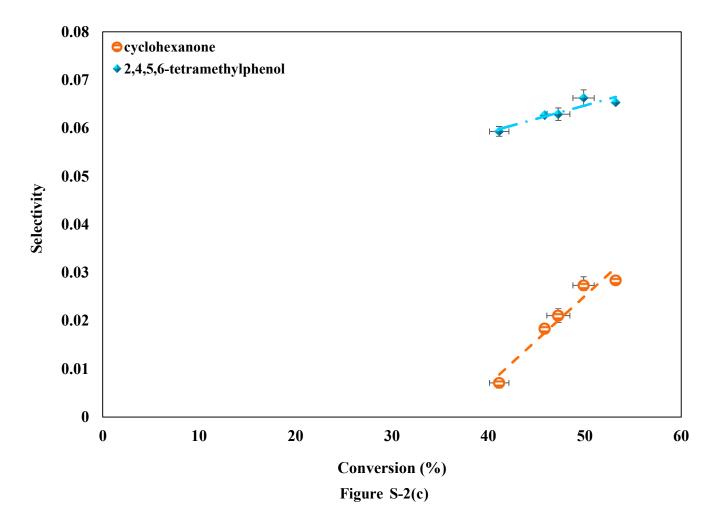


Figure S-2(b)



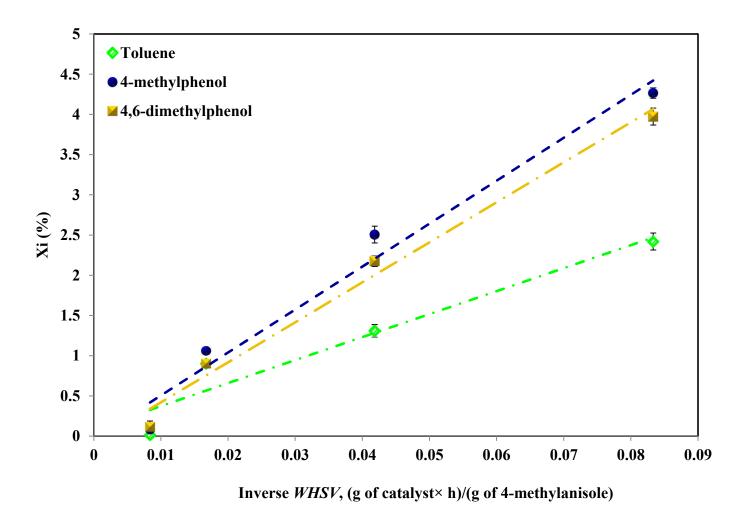


Figure S-3(a)

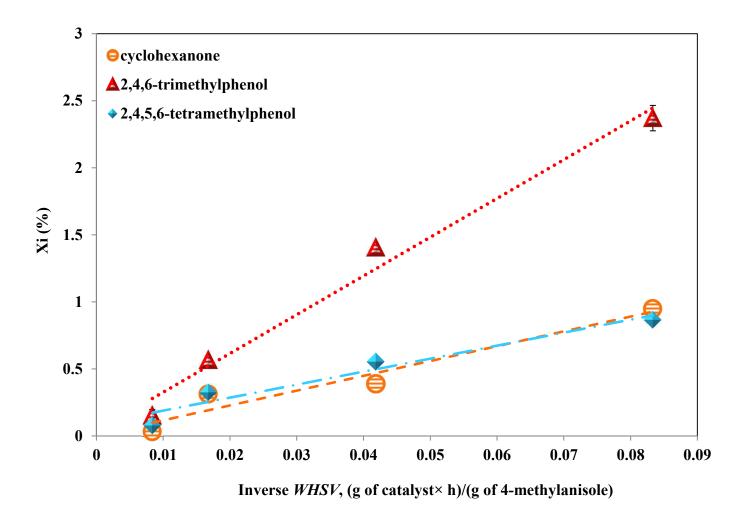


Figure S-3(b)

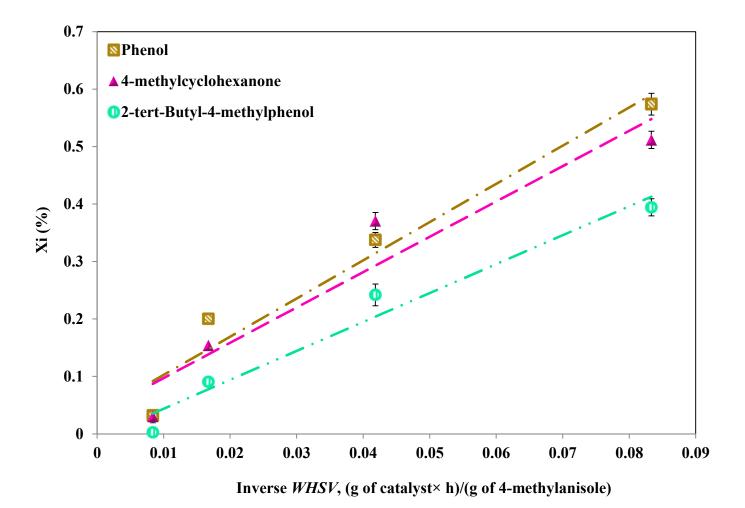
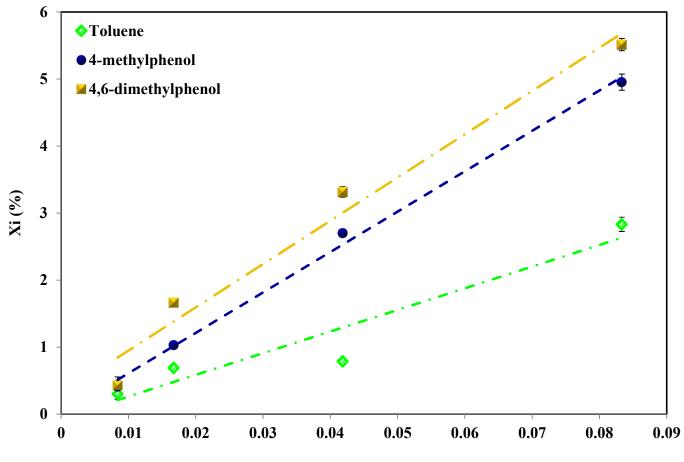


Figure S-3(c)



Inverse $W\!H\!SV$, (g of catalyst× h)/(g of 4-methylanisole)

Figure S-4(a)

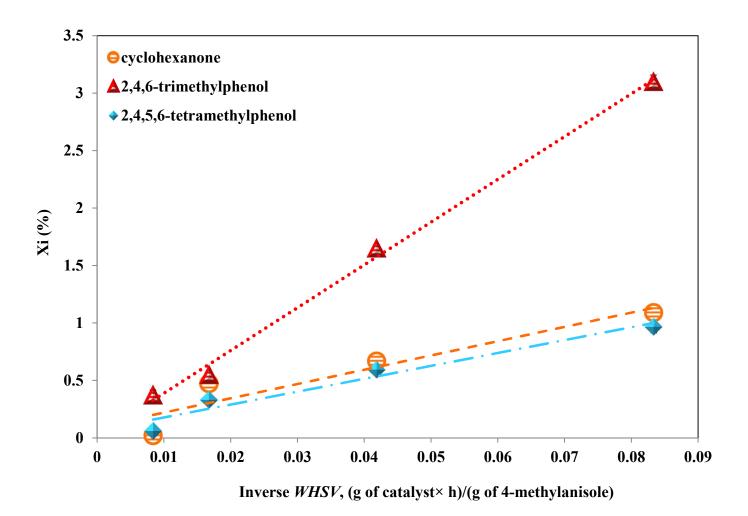
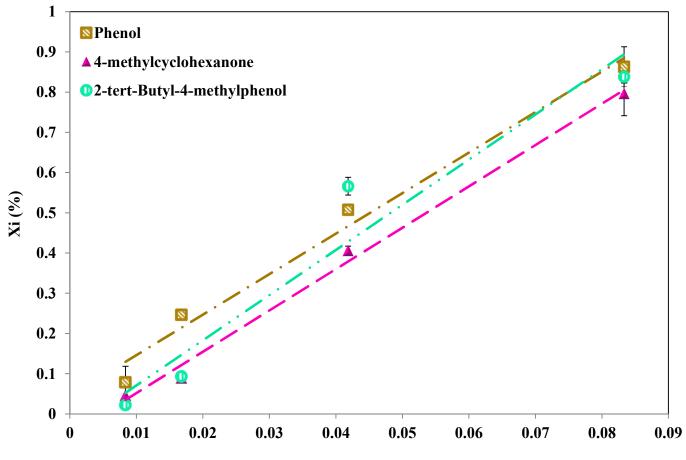


Figure S-4(b)



Inverse WHSV, (g of catalyst× h)/(g of 4-methylanisole)
Figure S-4(c)

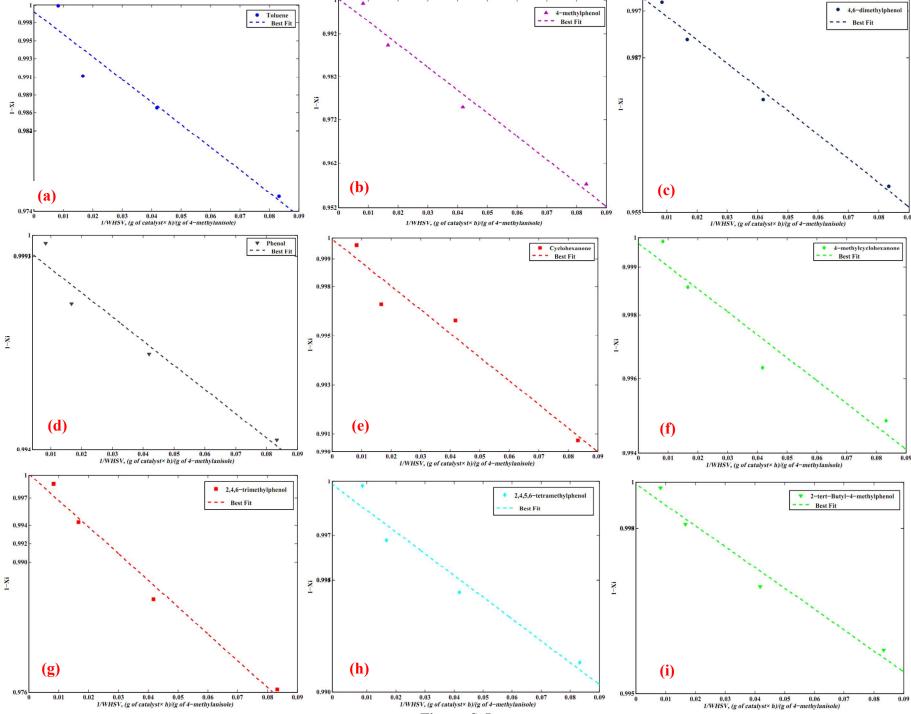


Figure S-5

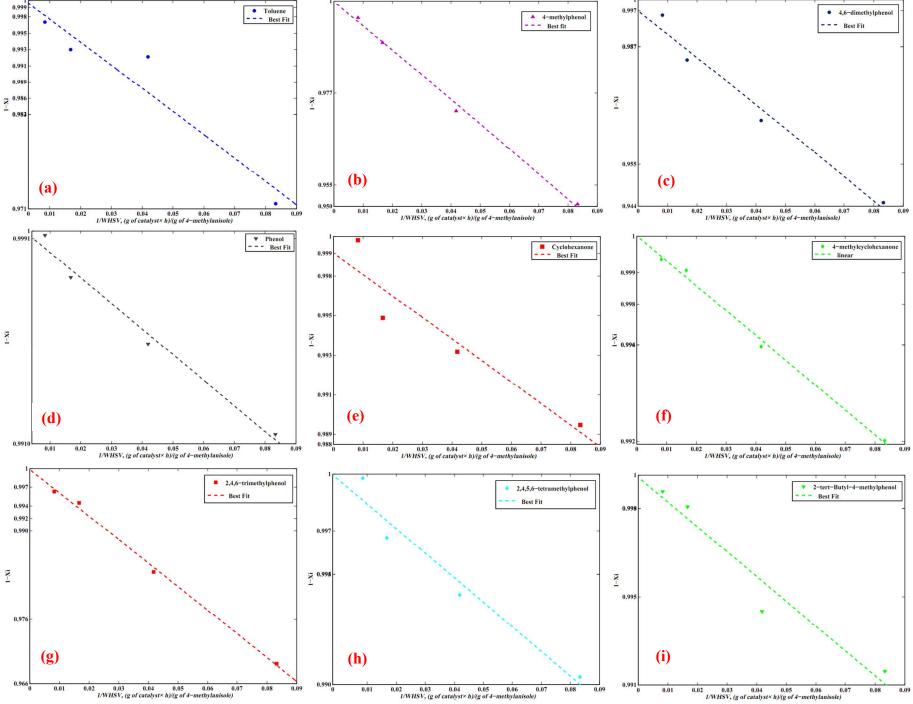


Figure S-6